CHAPTER 93

SOME CONSIDERATIONS ON HYDRAULIC DESIGN OF BOTTOM WATER INTAKE

Shin-ichi Senshu Supervisor, Coastal Hydraulic Division, Hydraulics Department, Technical Laboratory, Central Research Institute of Electric Power Industry, Tokyo, Japan

ABSTRACT

The selective withdrawal characteristics of bottom water intake placed on the sea bed for the condenser cooling system of steam power station are presented and several design methods are proposed The results of field observations are also shown.

INTRODUCTION

Recently in Japan, the most intake structures for condenser cooling system of thermal (or nuclear) power stations sited on a seashore are designed as bottom water intake in order to withdraw a large quantity of clean water of low temperature from the deep layer of thermally stratified sea basin. The following types have been used for such intake structures: (a) skimmer-wall type, (b) horizontal inlet of intake pipe, and (c) vertical inlet of intake pipe. (shown in Fig. 1) The characteristics of skimmer-wall type intake were previously studied by the author and the bottom water intake of this type has been constructed at several power stations

In this paper, the characteristics of horizontal type inlet of bottom water intake pipe are presented on the basis of fundamental experiments conducted at the Hydraulics Laboratory of CRIEPI and some design methods are proposed. The results of field observations are also shown which were carried out to examine the effect of bottom water withdrawal by such structures

CHARACTERISTICS OF HORIZONTAL TYPE INLET

The withdrawal characteristics of horizontal type inlet depend on the following values; (see Fig. I (b))

- b width of rectangular opening of inlet,
- ho height of opening,
- \varDelta · depth from interface of stratification to top of opening,
- z_o rise from sea bed to bottom of opening,
- $L\,\cdot\,$ topographical clearance behind opening (horizontal distance from opening to bank),
- L' length of visor horizontally projecting at the top of opening,
- ρ density of lower layer water,
- $\Delta \rho$ difference in density of two layers water,
- $Q_{\rm c}$ maximum discharge under critical condition, which can be taken from the lower layer water without drawdown of interface,
- u_o mean velocity at the opening under critical condition, $u_o = Q_c / bh_o$

Considering the effect of three-dimensional flow approaching the inlet, the critical withdrawal condition for the horizontal type inlet with rectangular opening can be obtained from the energy equation as follows

1442

where

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$$u_{0} = \frac{u_{0}}{\sqrt{g(\Delta \rho/\rho)h_{0}}}$$

In Eq. 1, c denotes the coefficient depending on the velocity distribution of approaching flow and should be determined experimentally as the function $l = L/h \circ$, $m = z \circ / h \circ$, $n = b / h \circ$ and $l = L/h \circ$

The value of c is shown in Fig. 2 (a) and (b), which is obtained from the experiment of three-dimensional. These figures correspond to the opening of rectangular section whose ratio of width to height is $4 \cdot 1$ (n = 4) However, the results of the experiment show that the effect of the opening geometry (ratio of width to height, n) on the withdrawal characteristics is not dominant for the r range of n = 2 - 4. For the considerably larger value of n, the value of c has a tendency to become smaller, since the effect of the three-dimensional inflow from the both sides of the opening declines and the two-dimensional inflow prevails. It is found from Fig. 2 (b) that the visor installed at the top of the opening is effectual on increasing the maximum discharge under the critical

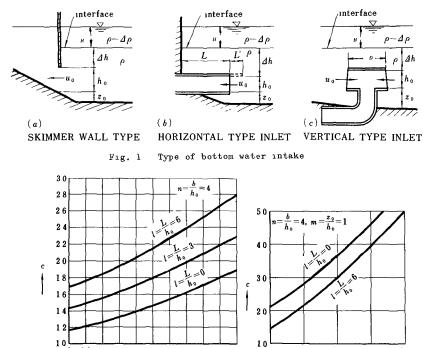


Fig 2. Value of coefficient, c, in Eq. 1.

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 $l' = L'/h_0$

(b)

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2.0

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 $0\ 2\ 0\ 4\ 0\ 6\ 0\ 8\ 1\ 0\ 1\ 2\ 1\ 4\ 1\ 6\ 1\ 8\ 2\ 0$

 $m = z_0 / h_0$

(a)

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HYDRAULIC DESIGN OF BOTTOM WATER INTAKE

1. Method of economical design to minimize the total depth

This method is based on the idea that the most economical size of the intake is given by the opening height λ_o so as to minimize the total depth below the interface, $z_0 + \lambda_o + 4\lambda$, for a given discharge under the critical condition. The economical opening height λ_o in this manner is obtained from Eq. 1 for horizontal type inlet, by differentiating $z_0 + \lambda_o + 4\lambda$ with respect to λ_o and equating to zero, that is

and the corresponding depth Ah is

The economical opening height, h_o , for skimmer-wall type intake can be obtained in the same manner from the critical withdrawal condition, $p_{i,o} = 0.9(dh/h_o)$, based on the result of the two-dimensional experiment presented in the author's previous study, as follows.

$$k_{o} = \left(\frac{q}{2 \times 09 \sqrt{g} \frac{d\rho}{\rho}}\right)^{2/3} \qquad \dots \qquad \dots \qquad \dots \qquad (4)$$

and the corresponding depth dh is

$$d\lambda = \frac{q}{\log \sqrt{g \frac{d\rho}{\rho} \lambda_o}} \quad \dots \qquad (5)$$

where, q is maximum discharge per unit width of skimmer-wall under the critical condition

Several examples of bottom water intake of horizontal type inlet designed by this method are shown in Table-1 in these examples, maximum intake discharge is $Q = 11 \text{ m}^3/\text{sec}$, depth of upper layer H = 4 m, and relative density difference $d\rho/\rho = 0.0017$ (corresponding to temperature difference between upper and lower layer water, $\Delta T = 5$ °C).

No.	Design condition	⊿h (m)	h		Total depth $H + \Delta h + h \circ + z \circ$ (m)	u . (m/s)
1	ι =6, m=0, ι'=0	3.23	2 16	0	9.39	0.590
2	ι=6, m=1, ι'=0	3.88	1.30	1.30	10.48	1.627
3	l=6, m=1.5, l'=0	4.04	1.08	1.62	10.74	2.360
4	l =6, m=0.5, l'=1	2.88	1.28	0.64	8.80	1.678

Table-1. Horizontal type inlet designed by the method to minimize total depth (n = 4).

2. Method of providing the inlet velocity so as to keep stability of the interface

The design method described above is apt to give rather large magnitude of inlet velocity, which promotes occurrence of turbulent mixing at the interface and results in simultaneous inflow from the upper layer. It would be the practical method, therefore, to determine the value of h_0 and 4h under the critical condition, by providing first the inlet velocity u_0 with the magnitude to keep stability of the interface.

For horizontal type inlet of rectangular opening $(b = nh_o)$,

and

$$\Delta h = \left(\frac{u \circ h_{\sigma}}{c \sqrt{g \frac{d \rho}{\rho}}}\right)^{2/3} \qquad \dots \qquad \dots \qquad (7)$$

It is adequately recommended that the magnitude of u_\circ should be taken as 0.10 \sim 0.20 m/sec, on the basis of stability condition of interface of two-layer stratification.

Figure 3 is the design diagram of horizontal type inlet by this method based on Eqs. 6 and 7 for the condition $\Delta\rho/\rho = 0.0017$ ($\Delta T = 5$ °C), n = 4, and c = 1 17 (l = 0, m = 0).

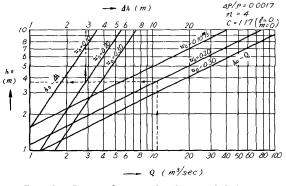


Fig. 3. Design diagram for horizontal type inlet by method of providing the inlet velocity.

For skimmer-wall type bottom water intake, the values of h_o and corresponding $\varDelta h$ for the given inlet velocity u_o are determined by

and

$$\Delta h = \left(\frac{u_o}{09\sqrt{g\frac{d\rho}{\rho}}}\right) h_o^{\frac{1}{2}} \qquad \dots \qquad \dots \qquad \dots \qquad \dots \qquad (9)$$

Several examples of bottom water intake of horizontal type inlet designed by this method are shown in Table-2 In these examples, the values of Q, H and $\Delta \rho / \rho$ are same as the ones for the above examples in Table-1

Table 2 Horizontal type and skimmer-wall type inlet designed by the method so as to keep stability of interface (inlet velocity, u., is given first).

No	Design condition	⊿h (m)	h	z. (m)	Total depth $B + \Delta h + h_{\sigma} + z_{\sigma}$ (m)	b (m)	Given inlet velocity u. (m/sec)
a-1	l = 0, m = 0, l' = 0	2 88	3.70	0	10 58	14 8	0 20
a-2	horizontal $l = 0, m = 0$ $l' = 0$	3 30	3.00	0	10 30	12 0	0 30
a3	type inlet, n = 4 $l = 6$, $m = 1$, $l' = 0$	1 92	3 70	370	13 32	14 8	0 20
a-4	$l = 6, m = 0 3, \tilde{l}' = 0.4$	1 82	3 70	1 11	10 63	14 8	0 20
Ь	Skimmer-wall type inlet (two-dimensional case of a-1)	3 32	3 72	0	11 04	14 8	0 20

3. Hydraulic design of vertical type inlet

The vertical type inlet with cover plate and bottom guide plate as shown in Fig. 1 (c), can be designed in the same manner by applying the above-mentioned methods for the horizontal type inlet to each divided portion around the opening

Divide the cylindrical opening formed between the upper cover plate and the lower glude plate of diameter D' into α portions (for each divided portion, $n = (\pi D^{1}/2)/h_{o}$), and apply the design formular to each portion of β among α , assuming that the remaining part ($\alpha - \beta$) is ineffectual for withdrawing water due to the surrounding obstruction.

For a given discharge Q and inlet velocity u_{\circ} , the opening height h_{\circ} is obtained from

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then, the corresponding depth Δh can be calculated by Eq. 7, in which the value of coefficient c should be taken for the case of l=0.

On the other hand, in the economical design to minimize the total depth at the inlet, the calculating formulas are as follows:

$$D = \left\{ \frac{2 \, n \alpha}{3 \, \pi (1+m)} \right\}^{\frac{q}{2}}_{5} \left(\frac{Q}{c \pi \frac{\beta}{\alpha} \sqrt{g \frac{d P}{\rho}}} \right)^{\frac{q}{2}}_{6} \qquad (11)$$

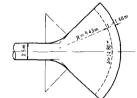
$$u_{o} = \frac{Q}{\pi D_{\alpha}^{\beta} k_{o}} \qquad . \tag{13}$$

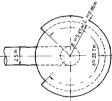
For a given discharge Q, the diameter of the cylindrical opening, D', is obtained from Eq. 11, then successively $h\circ$ from Eq. 12, $u\circ$ from Eq. 13 and dh from Eq. 7.

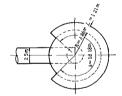
Two design examples of bottom water intake of vertical type inlet for the same value of Q, // and $d\rho\,/\,\rho\,$ as in examples above described, are shown in Table-3

Table-3. Vertical type inlet for the given inlet velocity, us = 0.20 m/sec

No	Design condition	 Dי (m)	⊿ħ (m)	ћ, (m)		Total depth $H + \Delta h + h \circ + z \circ$ (m)
c - 1	$\ell = 0, m = 0.5, \ell' = 0.4, n = 4, \alpha = 4, \beta = 3,$	10.90	1.48	2.14	1.07	8.69
c - 2	$l=0, m=0 3, l'=0.4, n=2, \alpha =4, \beta =3,$	7.72	1.90	3.03	0.91	9.85







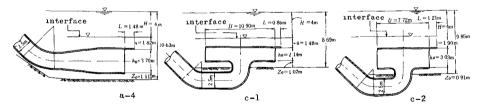


Fig. 4. Design examples of horizontal type and vertical type bottom water intake.

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These two vertical type bottom water intakes are sketched in Fig. 4, together with one example of horizontal type intake (a-4 in Table-2) Comparing c-1 with c-2, c-2 for n=2 is rather economical than c-1 for n=4, because the volume of the whole structure for the former is 2/3 of the one for the latter.

4 Method of permitting to entrain the surface layer water of high temperature beyond the critical condition

Above mentioned are the design methods to take the colder bottom water from the theimally stratified basin and to prevent the warmer surface water from withdrawing into the cooling system. However, when the flow rate increases and exceeds the maximum discharge under the critical condition, the interface is drawn down below the top of the opening and simultaneous inflow from the upper layer may develop.

To permit the entrainment of warmer water from the upper layer to some extent brings the design method to obtain more economical intake structures than designed under critical condition. In case of such a design method, the required depth dk for horizontal type inlet is estimated by the following equation for a given entrainment factor λ ;

in which, dhc is the depth for the critical design given by Eq. 7, and entrainment factor λ is the ratio of inflow from the upper layer to total discharge withdrawn through the opening. Mean water temperature of cooling water, τ_c , when warmer surface water is entrained, is estimated by

where T_1 and T_2 is water temperature in upper and lower layer, respectively

For two-dimensional skimmer-wall type intake, the following relation should be used, instead of Eq 14;

$$\Delta h = \Delta h c \left(1 - \lambda\right)^2 - \lambda h c \qquad (16)$$

Equation 15 or Eq. 16 can also be used to estimate the entrainment factor λ for the existing intake structures

FIELD OBSERVATIONS

To examine the effect of bottom water intake structures designed by the author's method, field observations have been carried out at several thermal power stations

Figure 5 shows an example of the observed vertical distributions outside and inside of the skimmer-wall type bottom water intake at SAKA1-KO Thermal Power Station sited in Osaka Bay The intake structure was completed in July of 1967. The maximum discharge of cooling water is 100 m³/sec for the output of 2000 MW in its final project. The opening height below the skimmer-wall, k_o , is 4.8 m, and the designing mean velocity at the opening, u_o , is 0 16 m/sec.

As seen in Fig. 5, the conspicuous stratification due to water temperature difference develops in the basin in front of the intake in August, and this bottom water intake is of great advantage to withdraw colder clean water. The average temperature of cooling water measured at the pumping pit was 24 $^{\rm O}{\rm C}$ in spite of the water temperature of 30.5 $^{\rm O}{\rm C}$ in surface layer outside of the skimmer-wall.

1448

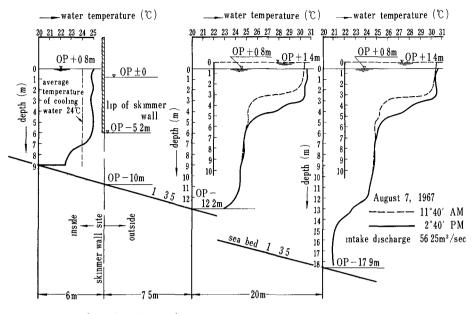


Fig. 5. Observed water temperature distribution at bottom water intake of cooling system for Sakai-ko Thermal Power Station

Figure 6 shows another example of vertical temperature distributions outside of the skimmer-wall type bottom water intake observed at SHIN-SHIMIZU Thermal Power Station sited in Shimizu Port. The maximum discharge of cooling water is 11.7 m³/sec for the total output of 306 MW, $\lambda_o = 4.12$ m and ω_o is 0.07 m/sec. The cooling water discharge during the testing period was 6.15 m³/sec.

Assuming the discontinuous temperature distribution outside of the skimmerwall shown by dotted line in Fig. 6, the average temperature of cooling water is calculated by the author's method as 25.85 °C ($\lambda = 6$ %) in ebb tide and 26.1 °C ($\lambda = 0$) in flood tide. These values are in quite agreement with the observed water temperature at pumping pit.

Figure 7 shows the water temperature distribution in front of the horizontal type bottom water intake with visor observed at ICHIHARA Thermal Power Station in Tokyo Bay Assuming that $T_1 = 26.5$ °C for upper layer, $T_2 = 21.5$ °C for lower layer, depth of surface layer H = 3.5 m from the observed temperature distribution on August 15, the average temperature of cooling water is estimated as 21.7 °C ($\lambda = 4.5\%$).

Figure 8 shows the water temperature distribution around the vertical type inlet of bottom water intake pipe for SAKAI PLANT of UBE KOSAN Industrical Company in Osaka Bay. It is seen that the conspicuous density stratification is formed near the intake. Assuming that $T_1 = 27.5$ °C, $T_2 = 24.3$ °C and H = 3.6 m from the observed data, calculation gives $\lambda = 0$. Therefore, water temperature of cooling water results in the assumed lower layer temperature, 24.3 °C, which coincides with the average temperature measured at the pumping pit.

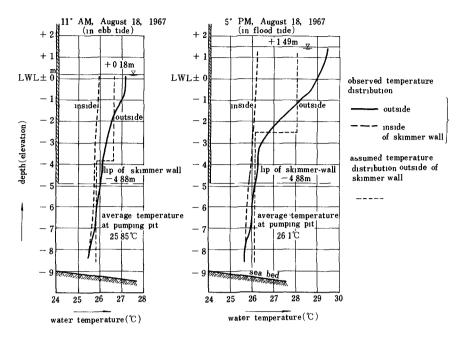


Fig. 6. Observed water temperature distribution at bottom water intake for SHIN-SHIMIZU Thermal Power Station.

Studies are further continued to make clear the characteristics of selective withdrawal in the field of continuous density distribution which is generally more actual condition in sea basin.

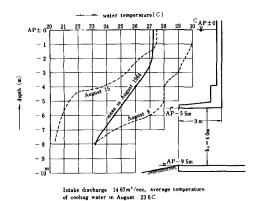


Fig. 7 An example of water temperature distribution observed in front of bottom water intake for ICHIHARA Thermal Power Station.

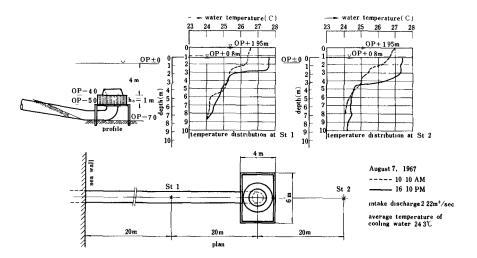


Fig. 8. Water temperature distribution observed at vertical type inlet of intake pipe for SAKAI PLANT of UBE KOSAN INDUSTRIAL COMPANY.

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REFERENCE

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